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Der Präsident des Europäischen Patentamts;
im Auftrag

For the President of the European Patent Office

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**The in situ polymerization of monoethylenically unsaturated monomers with
oligomeric or polymeric secondary amines**

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The in situ polymerization of monoethylenically unsaturated monomers with oligomeric or polymeric secondary amines

5 The present invention relates to a new process for the preparation of well-defined random and block polymers or copolymers using hindered secondary amine-oligomers or -polymers.

10 Today, the demand for homopolymers, random copolymers and block copolymers of a specific molecular weight, narrow molecular weight distribution and/or well-defined end groups has continuously increased in a number of industries. The controlled structure of these macromolecules provides them with novel properties and allows a tailor-made property profile to be obtained. Many new technologies require controlled polymer structures such as for instance in the fields of electronics,
15 computer science, communications, genetic engineering, biotechnology and materials science.

20 Many polymers are commercially produced by free radical polymerization due to the far less demanding conditions, i.e. the possible use of water as solvent, the far broader temperature range which can be employed as well as the broader range of monomers which can be polymerized. Moreover, radical copolymerization offers many opportunities for modifying the polymer properties. The neutrality of the radical species is however responsible for irreversible transfer and termination reactions, which are responsible for the poor control of the macromolecular structures
25 including degree of polymerization, polymolecularity, end functionality and chain architecture.

30 On the other hand, controlled radical polymerization (CRP) is a powerful tool for finely controlling the molecular characteristics of the chains (M_n , M_w/M_n) and their macromolecular architecture. For example, well-defined block copolymers can be synthesized by the sequential addition of comonomers and polymers with terminal

functional groups can be made available by the judicious choice of either the initiator (α -chain-end) or the deactivating agent (ω -chain-end).

5 Of all the CRP systems presently under investigation, nitroxyl-mediated polymerization is one of the most efficient. This process is based on the reversible capture of the propagating radicals by nitroxyl radicals to form dormant chains. This approach is for example disclosed in US-A 4,581,429. Nevertheless, this NMP process is handicapped by slow polymerization kinetics, a limited range of suitable monomers and the high cost of the required nitroxyl radicals.

10

Quite recently, some of these NMP problems have been solved. Both the acceleration of the rate of polymerization and the broadening of the range of monomers to be polymerized have been reported by Hawker et al. (*J. Am. Chem. Soc.* 1999, 121, 3904) and for example in WO-A 96/24620. Reduced polymerization temperatures
15 have been reported by Miura et al. (*Macromolecules* 2001, 34, 447) by using nitroxyl radicals with spiro structures.

20

Although these improved NMP processes represent attractive methods for obtaining new polymer structures, they still require the use of not readily available and complicated nitroxyl radicals and/or alkoxyamines, which considerably increase the total cost of a technical process. Consequently, there is still a need for more simple NMP processes for polymerizing a broad range of monomers.

25

WO-A 99/03894 and US-A 6,262,206 disclose the use of nitrones and nitroso compounds to control the radical polymerization of vinyl monomers. When these compounds were added to the radical polymerization of vinyl monomers, nitroxyl radicals were formed in-situ by reaction of the initiating radicals or propagating chains with the nitrones or nitroso compounds. The polymerization was thus controlled by an NMP mechanism.

30

The use of nitrones and nitroso compounds for promoting the free-radical polymerization of vinyl monomers controlled by in-situ NMP process has also been reported for example by D. F. Grishin et al., *Polymer Science, Ser. A*, 1999, 41(4), 401; D. F. Grishin et al, *Polymer Science, Ser. B*. 2000 42(7-8), 189; D. F. Grishin et al., *Russian Journal of Applied Chemistry* 2001, 74(3), 494; D.F. Grishin et al. *Mendeleev Commun.* 1999, 250; D. F. Grishin et al., *Russian Journal of Applied Chemistry* 2001, 74(9), 1594.

More recently, the controlled radical polymerization of styrene mediated by nitroso-tert-octane was reported by J.M. Catala et al., *Macromolecules* 2001, 34, 8654.

These in situ processes using nitroso compounds or nitrones allowed the avoidance of the tedious synthesis of the nitroxyl radicals. Nevertheless, these methods require the use of preformed reagents which may be toxic (especially in case of nitroso compounds), and most of them are still not readily available and have to be synthesized by special method.

US-A 6,320,007 and JP-A 08208714 describe the manufacture of thermoplastic polymers having narrow molecular weight distribution using an in situ NMP process, in which the stable nitroxyl radical is formed from a precursor substance in a reactor. The polymerization process occurs in two steps: firstly the nitroxyl radicals are formed from the precursor (secondary amine) and secondly, the nitroxyl radical is added to the polymerization of the vinyl monomer in order to form a thermoplastic polymer characterized by a narrow molecular weight distribution. In the two examples, 2,2,6,6-tetramethylpiperidine (TMP) is used as precursor for the nitroxyl radical, when combined with m-chloroperbenzoic acid or a mixture of hydrogen peroxide and sodium tungstate as the oxidizing agent. Drawbacks of these processes are the long reaction times to form the nitroxyl radical prior to polymerization and the use of free-radical initiators (such as benzoyl peroxide for instance) to initiate the polymerization, which makes a preliminary reaction between the monomer, the initiator and the nitroxyl radical necessary before polymerization. This is associated

with an increase in the cost of the process. Moreover, the polymerizations are very slow and require several days to be completed.

5 The object of the present invention was to provide a new synthetic pathway for the synthesis of homo- and copolymers of controlled molecular weight and controlled molecular structure. Such a process should be a simple and inexpensive method of controlling the free-radical polymerization of vinyl monomers that overcomes the drawbacks encountered in the prior art.

10 Surprisingly, it has now been found that it is possible to provide a process for the preparation of well-defined (co)polymers of controlled molecular weight, narrow polydispersity, high monomer conversion and controlled architecture, at relatively low temperatures and with short reaction times, if the polymerization of vinyl monomers is carried out in the presence of at least one hindered secondary amine
15 chemically bound to a polymer or oligomer and an oxidizing agent. The addition of a free-radical initiator before polymerization is only optional. Moreover, no preliminary reaction between the secondary amine and the oxidizing agent is required prior to the addition of the monomer(s), and the polymerization medium can be quite rapidly heated at the polymerization temperature without any preliminary reaction of
20 the products.

The object of the present invention is a process for producing oligomers, co-oligomers, polymers or block or random copolymers comprising

25 (I) mixing compounds consisting essentially of

a) at least one monoethylenically unsaturated monomer of the general formula (M),

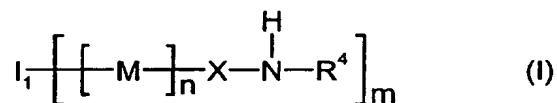
30
$$\text{HR}^1\text{C} = \text{CR}^2\text{R}^3 \quad (\text{M}),$$

wherein

R^1 , R^2 , R^3 are independently selected from the group consisting of hydrogen, C_1 - C_{20} -alkyl, C_1 - C_{20} -cycloalkyl, C_6 - C_{24} -aryl, halogen, cyano, C_1 - C_{20} -alkyl ester, C_1 - C_{20} -cycloalkyl ester, C_1 - C_{20} -alkylamide, C_1 - C_{20} -cycloalkylamide, C_6 - C_{24} -aryl ester and C_6 - C_{24} -arylamide,

b) at least one oxidizing agent (A) and

c) at least one polymer or oligomer containing at least one hindered secondary amine of the general formula (I),



wherein

R^1 , R^2 , R^3 have the aforesaid meaning,

m is an integer between 1 and 50, preferably between 1 and 20, and more preferably between 1 and 10,

n is an integer between 1 and 300, preferably between 1 and 50, and more preferably between 1 and 20 and

I_1 represents an initiator and

R^4 represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -

alkyl, C₂-C₁₈-alkenyl, C₂-C₁₈-alkynyl, C₃-C₁₂-cycloalkyl or C₃-C₁₂-heterocycloalkyl, C₆-C₂₄-aryl, which may be unsubstituted or substituted by NO₂, halogen, amino, hydroxy, cyano, carboxy, ketone, C₁-C₄-alkoxy, C₁-C₄-alkylthio or C₁-C₄-alkylamino,

5

X represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C₁-C₁₈-alkyl, C₂-C₁₈-alkenyl, C₂-C₁₈-alkynyl, C₃-C₁₂-cycloalkyl or C₃-C₁₂-heterocycloalkyl, C₆-C₂₄-aryl, which may be unsubstituted or substituted by NO₂, halogen, amino, hydroxy, cyano, carboxy, ketone, C₁-C₄-alkoxy, C₁-C₄-alkylthio or C₁-C₄-alkylamino,

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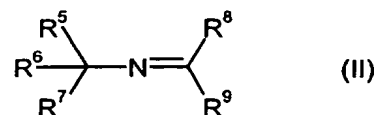
15 d) optionally in the presence of a free radical initiator (B) and

(II) then heating the mixture at a temperature in the range from about 0°C to 220°C.

20 The polymers or oligomers of the general formula (I) can be synthesized by any of the methods known in the prior art for synthesizing such functional polymers or oligomers .

25 Preferably, the synthesis of (I) is carried out by living anionic polymerization of one or several vinyl monomers followed by a capping reaction of the reactive anionic chains with imines of the general structure (II), as described, for example, in US-A 3,178,398 (column 5, lines 27-51) and US-A 4,816,520 (column 2, line 65 to column 3, line 7).

30 Suitable nitrogen compounds for the preparation of the polymers or oligomers of the general formula (I) are compounds of the general formula (II),



wherein

5 R^5 , R^6 and R^7 are independently selected from the group consisting of hydrogen, C_1 - C_{18} -alkyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -hetero-cycloalkyl and C_6 - C_{24} -aryl which is unsubstituted or substituted by C_1 - C_{18} -alkyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl;

10

wherein R^5 , R^6 and R^7 are bound to a secondary or tertiary carbon atom and can be identical or different;

15

R^5 , R^6 and R^7 optionally form, together with the intermediate carbon atom, a C_3 - C_{12} -cycloalkyl group or a C_2 - C_{13} -heterocycloalkyl group containing oxygen, sulfur or nitrogen atoms;

20

R^5 , R^6 and R^7 optionally form, together with the intermediate carbon atom, a C_6 - C_{24} -aryl or C_6 - C_{24} -heteroaryl residue containing oxygen, sulfur or nitrogen atoms;

25

R^5 , R^6 and R^7 optionally together form a residue of a polycyclic ring system or a polycyclic heterocycloaliphatic ring system containing oxygen, sulfur or nitrogen atoms;

R^8 and R^9 are independently selected from the group consisting of hydrogen, C_1 - C_{18} -alkyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -hetero-cycloalkyl and C_6 - C_{24} -aryl, which is unsubstituted or

substituted by C₁-C₁₈-alkyl, C₃-C₁₂-cycloalkyl or C₃-C₁₂-heterocycloalkyl.

5 Preferred nitrogen compounds are N-benzylidene-N-(tert-butyl)amine, N-(tert-butyl)-N-(2,2-dimethylpropylidene)amine, N-(tert-butyl)-N-(2-methylpropylidene)amine, N-(tert-butyl)-N-ethylideneamine, N-(tert-butyl)-N-(1-methylethylidene)amine, N-(2,2-dimethylpropylidene)-N-isopropylamine, N-isopropyl-N-(2-methylpropylidene)-amine, N-benzylidene-N-isopropylamine, N-isopropyl-N-(1-phenylethylidene)amine, N-(tert-butyl)-N-(1-phenylethylidene)amine and N-benzylidene-N-(phenyl)amine.

10

Particular preferred are N-benzylidene-N-(tert-butyl)amine, N-benzylidene-N-(phenyl)amine, N-benzylidene-N-isopropylamine and N-(tert-butyl)-N-(1-methylethylidene)amine.

15 The monomers which can be used for the preparation of polymers or oligomers of the general structure (I) using living anionic polymerization include conjugated dienes and vinyl-substituted aromatic compounds as reported in US-A 3,178,398 (column 2, line 30 to column 3, line 54) and US-A 4,816,520 (column 1, line 56 to column 2, line 2). Conjugated dienes can be polymerized alone or in admixture with each other
20 to form copolymers or block copolymers. Vinyl-substituted compounds can be polymerized alone or in admixture with each other to form copolymers or block copolymers. Vinyl-substituted compounds and conjugated dienes can be polymerized alone or in admixture with each other to form copolymers or block copolymers.

25 Styrene and styrene derivatives such as α -methylstyrene are the preferred monomers for the synthesis of the polymers or oligomers of the general formula (I).

Suitable initiators (I₁) can be any of the anionic initiators reported in US-A 3,178,398 (column 4, line 29 to column 5, line 26) and any of the initiators known in the prior
30 art for the anionic polymerization of vinyl monomers and dienes.

Multifunctional initiators well-known in the prior art can also be used. Examples of difunctional initiators include the naphthalene radical anion as reported by Szwarc et al. in *J. Am. Chem. Soc.* (1956, 78, 2656) and a combination of n-butyllithium (BuLi) and divinylbenzene (DVB) (Beinert et al., *Makromol. Chem.* 1978, 179, 551; Lutz et al., *Polymer* 1982, 23, 1953). By varying the ratio BuLi/DVB, it is also possible to form multifunctional initiators.

Typical monoethylenically unsaturated monomers (M) which are suitable for the process according to the present invention are the alkyl esters of acrylic or methacrylic acids, such as methyl acrylate, ethyl acrylate, butyl acrylate, methyl methacrylate, ethyl methacrylate, butyl methacrylate and isobutyl methacrylate; the hydroxyalkyl esters of acrylic or methacrylic acids, such as hydroxyethyl acrylate, hydroxypropyl acrylate, hydroxyethyl methacrylate and hydroxypropyl methacrylate; acrylamide, methacrylamide, N-tertiary butylacrylamide, N-methylacrylamide, N,N-dimethylacrylamide; acrylonitrile, methacrylonitrile, allyl alcohol, dimethylaminoethyl acrylate, dimethylaminoethyl methacrylate, phosphoethyl methacrylate, N-vinylpyrrolidone, N-vinylformamide, N-vinylimidazole, vinyl acetate, conjugated dienes such as butadiene or isoprene, styrene, styrenesulfonic acid salts, vinylsulfonic acid salts and 2-acrylamido-2-methylpropane-sulfonic acid salts and acryloyl. Suitable monomers (M) can be water-soluble or water-insoluble.

Examples of comonomers suitable for use in the present invention are C₃-C₆-ethylenically unsaturated monocarboxylic acids as well as the alkali metal salts and ammonium salts thereof. The C₃-C₆-ethylenically unsaturated monocarboxylic acids include acrylic acid, methacrylic acid, crotonic acid, vinylacetic acid and acryloxypropionic acid. Acrylic acid and methacrylic acid are the preferred monoethylenically unsaturated monocarboxylic acid monomers.

Examples of C₈-C₁₆-ethylenically unsaturated phenolic compounds which may also be used as comonomers are 4-hydroxystyrene, 4-hydroxy, α -methyl styrene, 2,6-ditert-butyl and 4-vinyl phenol.

Another class of carboxylic acid monomers suitable for use as comonomers in this invention are C₄-C₆-ethylenically unsaturated dicarboxylic acids and the alkali metal and ammonium salts thereof as well as the anhydrides of cis-dicarboxylic acids.

5 Suitable examples include maleic acid, maleic anhydride, itaconic acid, mesaconic acid, fumaric acid and citraconic acid. Maleic anhydride (and itaconic acid) is/are the preferred monoethylenically unsaturated dicarboxylic acid monomer(s).

10 The acid monomers suitable for use in the present invention may be in the form of their acids or in the form of the alkali metal salts or ammonium salts of the acid.

Preferred monomers are selected from the group consisting of (meth)acrylic acid esters of C₁-C₂₀-alcohols, acrylonitrile, cyanoacrylic acid esters of C₁-C₂₀-alcohols, maleic acid diesters of C₁-C₆-alcohols, maleic anhydride, vinylpyridines, vinyl-

15 (alkylpyrroles), vinyloxazoles, vinyloxazolines, vinylthiazoles, vinylimidazoles, vinylpyrimidines, vinyl ketones, styrene or styrene derivatives which contain a C₁-C₆-alkyl radical or halogen in the α -position and contain up to 3 additional substituents on the aromatic ring.

20 Particularly preferred monomers are styrene, substituted styrene, conjugated dienes, acrolein, vinyl acetate, acrylonitrile, methyl acrylate, methyl methacrylate, butyl acrylate, butyl methacrylate, 2-ethylhexyl acrylate, cyclohexyl methacrylate, isobornyl methacrylate and maleic anhydride.

25 Suitable oxidizing agents (A) for the process according to the present invention can be all oxidizing agents known from the prior art for the oxidation of secondary amines into nitroxyl radicals. Preferred oxidizing agents are peracids such as peracetic acid, perpropionic acid, m-chloroperbenzoic acid, dimethyldioxirane, perbenzoic acid or peroxides such as potassium peroxymonosulfate (2

30 KHSO₅·KHSO₄·K₂SO₄, Oxone[®], DuPont Specialty Chemistry, USA), hydrogen peroxide, hydrogen peroxide/sodium tungstate, hydrogen peroxides/titanium

containing catalysts, such as for example titanium dioxide and titanium silicalites (EP-A 0 488 403, page 5), phosphotungstic acid and oxidizing gases such as molecular oxygen or ozone.

- 5 Metal oxides such as silver oxide, lead (IV) oxide and sodium tungstate can also be used, optionally in combination with another oxidizing agent. A mixture of various oxidizing agents can also be used.

10 Particularly preferred are peracetic acid, perpropionic acid, hydrogen peroxide, hydrogen peroxide/titanium containing catalysts, potassium peroxy monosulfate ($2\text{KHSO}_5\cdot\text{KHSO}_4\cdot\text{K}_2\text{SO}_4$), silver oxide and lead (IV) oxide.

15 Suitable free radical initiators (B) of the present invention are any suitable agents producing free radicals, for example precursors such as azo compounds, peroxides or peroxy esters, which generate radicals by thermolysis or precursors such as styrene, which generate radicals by autopolymerization. It is also possible to generate radicals by redox systems, photochemical systems or by high energy radiation such as beam or X- or γ - radiation.

20 Other useful systems for generating radicals are organometallic compounds such as Grignard reagents (e.g. Hawker et al., *Macromolecules* 1996, 29, 5245) or halogenated compounds which produce radicals in the presence of a metal complex according to the Atom Transfer Radical Addition Process (ATRA) (e.g. WO-A 00/61544).

25 Examples of free radical initiators (B) generating free radicals by thermolysis are 2,2'-azobis(isobutyronitrile) (AIBN), 2,2'-azobis(isovaleronitrile), 2,2'-azobis(methylisobutyrate), 4,4'-azobis(4-cyanopentanoic acid), 1,1'-azobis(1-cyclohexanecarbonitrile), 2-tert-butylazo-2-cyanopropane, 2,2'-azobis[2-methyl-N-(1,1-bis-
30 (hydroxymethyl)-2-hydroxyethylpropionamide], 2,2'-azobis[2-methyl-N-(2-hydroxyethyl) propionamide], 2,2'-azobis(isobutyramidine hydrochloride), 2,2'-azobis(N,N'-

dimethyleneisobutyramine), 2,2'-azobis[2-methyl-N-(1,1-bis(hydroxymethyl)-2-ethyl)-propionamide], 2,2'-azobis[2-methyl-N-(2-hydroxyethylpropionamide)], 2,2'-azobis(isobutylamide) dihydrate, 2,2'-azobis(2,2,4-trimethylpentane), 2,2'-azobis(2-methylpropane), tert-butylperoxyacetate, tert-butylperoxybenzoate, tert-butylperoxyoctoate, tert-butylperoxyneodecanoate, tert-butylperoxyisobutyrate, tert-amylperoxypivalate, tert-butylperoxypivalate, diisopropylperoxydicarbonate, dicyclohexylperoxydicarbonate, dicumyl peroxide, dibenzoyl peroxide, di-tert-butylperoxide, dilauroylperoxide, potassium peroxydisulfate, ammonium peroxy disulfate, di-tert-butyl hyponitrite and dicumyl hyponitrite.

Initiators generating radicals by photolysis are for example benzoin derivatives, benzophenone, acyl phosphine oxides and photoredox systems.

Initiators generating radicals as a result of a redox reaction are in general a combination of an oxidant and a reducing agent. Suitable oxidants are, for example, tert-butyl hydroperoxide, cumyl hydroperoxide, benzoyl peroxide and p-methanehydroperoxide. Suitable reducing agents are for example Fe(II) salts, Ti(III) salts, potassium thiosulfate, potassium bisulfite, ascorbic acid and salts thereof, oxalic acid and salts thereof, dextrose and Rongalite® (sodium formaldehyde sulfoxylate, BASF AG, Ludwigshafen, Germany).

Preferred radical initiators (B) are compounds which generate free radicals by thermolysis. AIBN and benzoyl peroxide are particularly preferred.

One method of carrying out the process of the invention is that in the first step at least one polymer or oligomer of the general formula (I), at least one oxidizing agent (A) and at least one vinyl monomer (M) are mixed together. The temperature of the reaction may range from about -20°C to about 150°C, preferably from about 0°C to about 80°C, and more preferably from about 0°C to about 50°C. The reaction time may range from about 1 minute to about 72 h, preferably from about 5 minutes to about 24 h and more preferably from about 15 minutes to about 12 h. The first step of

the process of the present invention can be carried out in air or in an inert gas atmosphere such as nitrogen or argon.

5 The polymer or oligomer of the general formula (I) and the oxidizing agent (A) are introduced in a quantity ranging from about 40 wt.% to about 0.01 wt.%, preferably from about 20 wt.% to about 0.05 wt.% and more preferably from about 10 wt.% to about 0.1 wt.%, based on the weight of the monomer(s). The oxidizing agent (A) is introduced in a quantity ranging from about 0.01 to about 10 equivalents compared to the secondary amines groups contained by (I), preferably in a quantity from about 0.1
10 to about 2.5 equivalents, and more preferably in a quantity from about 0.2 to about 1.5 equivalents.

In the second step of the process according to the invention, polymerization occurs by heating the mixture of the first step at a temperature ranging from about 0°C to about 220°C, preferably from about 50°C to about 180°C, and most preferably from
15 about 70°C to about 150°C. The second step of the process of the present invention is generally carried out in an inert gas atmosphere such as nitrogen or argon. The reaction time may range from about 10 minutes to about 72 h, preferably from about 30 minutes to about 32 h and more preferably from about 1h to about 24 h.

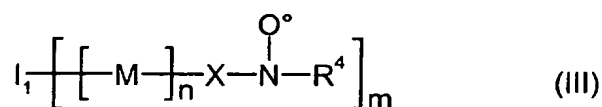
20 Optionally, a quantity of free radical initiator (B) can be added to the polymerization medium during the first step of the process and/or the second step of the process. The free radical initiator is introduced in a quantity ranging from about 0.01 to about 10 equivalents in relation to the polymer or oligomer of the general formula (I), preferably from about 0.1 to about 5 equivalents, and more preferably in a quantity
25 from about 0.2 to about 2 equivalents.

Another method of carrying out the process according to the invention is to heat a well-defined mixture of at least one polymer or oligomer of the general formula (I),
30 at least one oxidizing agent (A) and at least one vinyl monomer (M). The temperature ranges from about 0°C to about 220°C, preferably from about 50°C to about 180°C,

and most preferably from about 70°C to about 150°C. Polymerization is generally carried out in an inert gas atmosphere such as nitrogen or argon. The reaction time ranges from about 10 minutes to about 72 h, preferably from about 30 minutes to about 32 h, and more preferably from about 1h to about 24 h.

5

Another method of carrying out the process of the invention is to produce nitroxyl radicals of the general formula (III),



10 wherein

R^1 , R^2 , R^3 are independently selected from the group consisting of hydrogen, C_1 - C_{20} -alkyl, C_1 - C_{20} -cycloalkyl, C_6 - C_{24} -aryl, halogen, cyano, C_1 - C_{20} -alkyl ester, C_1 - C_{20} -cycloalkyl ester, C_1 - C_{20} -alkylamide, C_1 - C_{20} -cycloalkylamide, C_6 - C_{24} -aryl ester or C_6 - C_{24} -arylamide,

15

m is an integer between 1 and 50, preferably between 1 and 20, and more preferably between 1 and 10,

n is an integer between 1 and 300, preferably between 1 and 50, and more preferably between 1 and 20 and

I_1 represents an initiator and

R^4 represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -alkyl, C_2 - C_{18} -alkenyl, C_2 - C_{18} -alkynyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl, C_6 - C_{24} -aryl, which may be unsubstituted or substituted by NO_2 , halogen, amino, hydroxy, cyano, carboxy, ketone, C_1 - C_4 -alkoxy, C_1 - C_4 -alkylthio or C_1 - C_4 -alkylamino,

25

X represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C₁-C₁₈-alkyl, C₂-C₁₈-alkenyl, C₂-C₁₈-alkynyl, C₃-C₁₂-cycloalkyl or C₃-C₁₂-heterocycloalkyl, C₆-C₂₄-aryl, which may be
5 unsubstituted or substituted by NO₂, halogen, amino, hydroxy, cyano, carboxy, ketone, C₁-C₄-alkoxy, C₁-C₄-alkylthio or C₁-C₄-alkylamino,

by mixing the polymer or oligomer of the general structure (I) with the oxidizing agent (A), followed by isolation of the compound of the general formula (III).

10

The temperature of the first reaction step may range from about -20°C to about 150°C, preferably from about 0°C to about 80°C, and more preferably from about 0°C to about 50°C. The reaction time may range from about 1 minute to about 72 h, preferably from about 5 minutes to about 24 h and more preferably from about 15
15 minutes to about 12 h. The first step of this process can be carried out in air or in an inert gas atmosphere such as nitrogen or argon. Preferably, this reaction is carried out in the presence of solvents such as dichloromethane, toluene or xylene. Water can also be used as a cosolvent. When water is used as a cosolvent, a basic organic or inorganic buffer or organic or inorganic bases, such as Na₂CO₃, NaHCO₃, K₂CO₃, KHCO₃, Na₃PO₄, Na₂HPO₄, NaH₂PO₄, K₃PO₄, K₂HPO₄ or KH₂PO₄, sodium or
20 potassium hydrogen phthalate, metals salts of carboxylic acids such as acetic acid, propionic acid, exolic acid, phthalic acid or mixtures thereof, can be added. Preferred bases are Na₂CO₃, NaHCO₃, K₂CO₃, KHCO₃ or the sodium, calcium or potassium salt of acetic acid.

25

The molar ratio of oxidizing agent (A) to compounds of the general formula (I) is between 0.01 and 50, preferably between 0.1 and 20 and more preferably between 0.25 and 10. The polymer or oligomer of the general structure (I) and oxidizing agent (A) are introduced in a quantity ranging from about 80 wt.% to about 0.01 wt.%,
30 preferably from about 20 wt.% to about 0.1 wt.% and more preferably from about 10 wt.% to about 0.5 wt.%, based on the weight of the solvent. The polymer or

oligomer of the general formula (III) is finally recovered after synthesis and optionally purified.

5 In the second step of this process, the polymer or oligomer of the general formula (III) as prepared in step one, is dissolved in the vinyl monomer(s) (M) and the polymerization occurs by reacting this mixture at a temperature ranging from about 0°C to about 220°C, preferably from about 50°C to about 180°C, and most preferably from about 70°C to about 150°C. The second step of this process is generally carried out in an inert gas atmosphere such as nitrogen or argon. The
10 reaction time may range from about 10 minutes to about 72 h, preferably from about 30 minutes to about 32 h and more preferably from about 1h to about 24 h.

Optionally, a quantity of free radical initiator (B) can be added to the polymerization medium during the second step of the process. The free radical initiator is introduced
15 in a quantity ranging from about 0,01 to about 10 equivalents in relation to (I), preferably from about 0.1 to about 5 equivalents, and more preferably from about 0.2 to about 2 equivalents.

The present invention also relates to a polymerizable composition containing
20 a) at least one vinyl monomer or ethylenically unsaturated oligomer,
b) at least one polymer or oligomer of the general formula (III), and
c) optionally a free radical initiator (B).

In the process according to the invention it is preferred to use as few solvents as
25 possible. If organic solvents are required, suitable solvents or mixtures of solvents are typically pure alkanes, such as hexane, heptane or cycloalkane, hydrocarbons, such as toluene, ethylbenzene or xylene, halogenated hydrocarbons, such as chloro-
benzene, esters, such as ethyl acetate, propyl, butyl or hexyl acetate, ethers, such as diethyl ether, dibutyl ether or ethylene glycol dimethyl ether, alcohols, such as
30 methanol, ethanol, ethylene glycol, monomethyl ether, ketones, amides, sulfoxides or

mixtures thereof. Water can also be used in the process according to the present invention.

5 Water can be used in the process of the present invention when water-soluble monomers are used. Water can also be used for the polymerization of water-insoluble monomers in order to provide emulsion, miniemulsion, suspension or dispersion polymerization.

10 The type of polymerization used can be bulk, solution, miniemulsion, emulsion, dispersion or suspension polymerization and it can be carried out either batchwise, semi-batchwise or continuously.

15 Optionally, some additives can be added to the polymerization medium before the polymerization or during the polymerization process in order to accelerate the polymerization. Such additives are well-known in the art and are for example camphorsulfonic acid, 2-fluoro-1-methylpyridinium p-toluenesulfonate, acylating compounds such as acetic anhydride (Tetrahedron 1997, 53(45), 15225), glucose, dextrose (Macromolecules 1998, 31, 7559), ascorbic acid (Macromolecules 2001, 34, 6531) or long-life radical initiators as reported in US-A 6,288,186 (column 4, lines 8-20 24).

The polymers prepared according to the present invention display low polydispersity (M_w/M_n) which is usually lower than 2 and preferably lower than 1,5.

25 The number average molecular weight of the polymer chains increases linearly with the monomer conversion, which allows a tailor-made polymer molecular weight to be obtained. Furthermore, the molecular weight of the polymers can be controlled by varying the amount of secondary amine(s) (compound (I)) and/or oxidizing agent(s) in relation to the amount of monomers. High molecular weight polymers can be 30 formed.

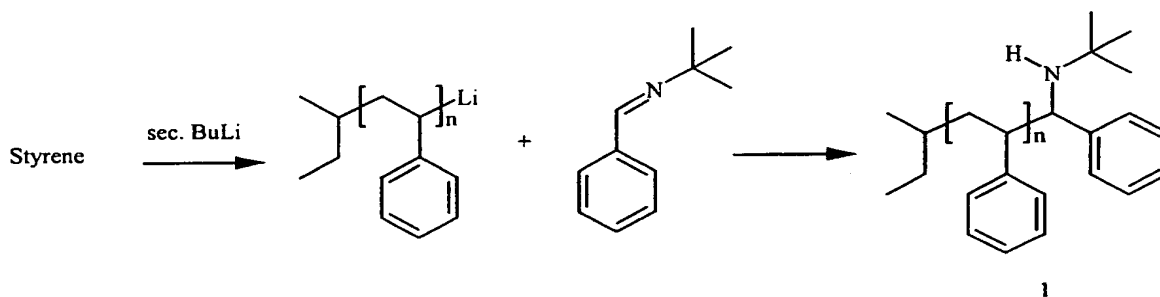
A further advantage of the present invention is that, after the removal of the non-polymerized monomers from the (co)polymers or after reaching a conversion rate of 100%, a second polymerization step can be initiated simply by adding to the polymer synthesized in the first step more of fresh vinyl monomer or monomer mixture that
5 can be different from the vinyl monomer or monomer mixture used in the first polymerization step. The polymerization of the vinyl monomer or monomer mixture added in the second step is then initiated by the polymer chains synthesized in the first polymerization step and di-block copolymers can, for example, be produced if the polymer chains synthesized in the first polymerization step consist of linear
10 chains with one single growing chain end. The molecular weight and polydispersity of each block can be controlled independently during the respective polymerization step. This process can be repeated several times and can then provide multiblock copolymers of controlled molecular weight and molecular weight distribution for each block.

15 The following examples illustrate the invention in more detail.

Examples

The molecular weight was determined by gel permeation chromatography (GPC) using a Shodex RI 74 differential refractometer. A flow rate of 1 ml/min was used and samples were prepared in THF. Polystyrene standards were used for calibration.

Example 1: Anionic synthesis of a polystyrene terminated by N-benzylidene-tert-butylamine



Drying of the vessel:

To a 300 ml four-necked flat-bottomed flask fitted with a mechanical stirrer, a reflux condenser and a thermometer are added distilled cyclohexane (100 ml) and styrene (1 g) under an argon atmosphere. The temperature is then heated at 60°C and 2 ml of sec-butyllithium (Aldrich; 1.3 M) are added. The polymerization medium becomes orange and after 30 minutes, the polymerization medium is removed. Then, the reactor is filled with argon and washed with 50 ml of distilled cyclohexane.

Polymerization:

To the dried reactor 200 ml cyclohexane and 10 g of styrene (0.096 mol) are added, and the temperature is increased to 50°C under an argon atmosphere. The polymerization of styrene is initiated by the addition of 7.69 ml of sec-butyllithium (Aldrich; 1.3 M; 0.01 mol). The polymerization medium becomes orange and the temperature increases to 60.4°C (in a slightly exothermic reaction). After a reaction time of 1 h, the temperature is 50.5°C and 1.61 g of N-benzylidene-tert-butylamine

(0.01 mol) is added. The polymerization medium becomes rapidly colourless. After 30 minutes at 50.5°C, 0.77 ml of isopropanol (0.01 mol) is added. The organic solution is then washed 3 times with 100 ml of water, dried with Na₂SO₄, filter and finally, the solvent and residual monomer are removed in vacuo at 70°C. The
5 polymer is dissolved in 100 ml of cyclohexane, washed twice with 150 ml 1N HCl and once with water. Finally, cyclohexane is removed in vacuo at 70°C and 9.36 g of **1** are collected as a white solid.

The molecular characteristics of **1** as measured by GPC:

10

Mn = 1136 g/mol

Mw = 1236 g/mol

Mw/Mn = 1.09

15 **Example 2:** Copolymerization of styrene and acrylonitrile in the presence of **1** synthesized in Example 1 and peracetic acid, according to the present invention

To a 100 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a
20 reflux condenser, a thermometer and a funnel is added 0.192 g of peracetic acid (Aldrich, 35 wt.%; $8.83 \cdot 10^{-4}$ mol). Then, a mixture of 1 g of **1** ($8.83 \cdot 10^{-4}$ mol, calculated from the number average molecular weight Mn of **1** as determined by GPC), 14.67 g styrene (0.141 mol) and 4.89 g acrylonitrile (0.092 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon
25 for 10 minutes. After 30 minutes at room temperature, the mixture is heated under reflux for 2.33 h. Samples are extracted from the reaction flask after 2 h and 2.33 h and dried in vacuo at 70°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC. Table 1 shows the results obtained by GPC.

30

Table 1: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
2	64.5	46330	65270	1.41
2.33	89.5	53460	78310	1.47

The increase in the molecular weight of the polymer with the monomer conversion rate and the narrow polydispersity are consistent with a controlled process.

Additionally, the polymerization of SAN in the presence of **1** and peracetic acid, in the absence of any additional initiator, takes place very quickly and is almost complete after 2.5 h.

Comparative example A: Polymerization of styrene/acrylonitrile in the presence of peracetic acid and in the absence of **1**.

To a 100 ml four-necked round bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel is added 0.192 g of peracetic acid (Aldrich, 35 wt.%; $8.83 \cdot 10^{-4}$ mol). Then, a mixture of 14.67 g of styrene (0.141 mol) and 4.89 g of acrylonitrile (0.092 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at room temperature, the mixture is heated under reflux for 45 minutes. The polymer is dissolved in chloroform, precipitated in methanol and then dried in vacuo at 50°C. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC. Table 2 shows the results obtained by GPC.

Table 2: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
0.75	94.5	116400	276100	2.37

The polymerization in the absence of **1** takes place very rapidly and in an un-
controlled manner. A high molecular weight polymer and very broad polydispersity
are obtained.

Comparative example B: Polymerization of styrene/acrylonitrile in the presence
of 2,2,6,6-tetramethylpiperidine-1-oxyl (TEMPO)

To a 100 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a
reflux condenser, a thermometer and a funnel is added a mixture of 14.67 g styrene
(0.141 mol), 4.89 g acrylonitrile (0.092 mol) and 0.137 g TEMPO ($8.8 \cdot 10^{-4}$ mol)
rapidly via the funnel. The mixture is stirred and degassed by bubbling through argon
for 10 minutes. After 30 minutes at room temperature, the mixture is heated under
reflux for 24 h. Samples are extracted from the reaction flask after 2 h and 24 h and
dried in vacuo at 70°C for 24 h. The monomer conversion is determined by
gravimetric analysis and the molecular weight of the polymer is determined by GPC.

Table 3 shows the results obtained by GPC.

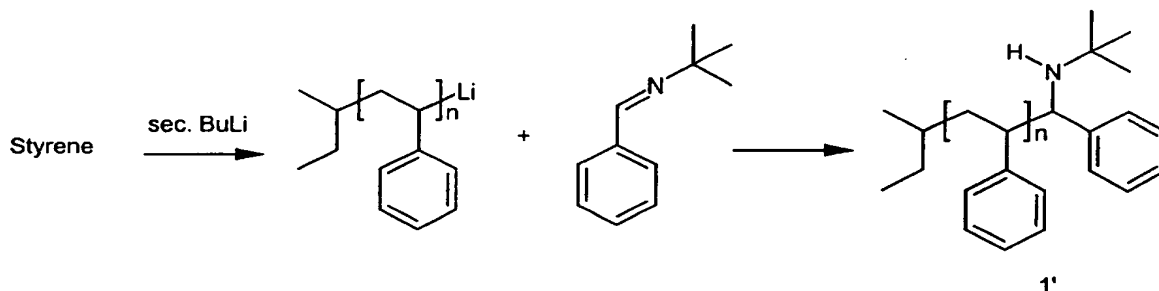
Table 3: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
2	0	-	-	-
24	55.1	9400	13140	1.39

When using the same molar amount of TEMPO ($8.8 \cdot 10^{-4}$ mol) as of **1** ($8.8 \cdot 10^{-4}$ mol), the polymerization of SAN is much slower in the presence of TEMPO compared to the polymerization of SAN in the presence of a combination of **1** and peracetic acid.

Indeed, an only 55 % monomer conversion is obtained after 24 h at reflux in the presence of TEMPO compared to a 89.5 % monomer conversion after 2,33 h in the presence of **1** and peracetic acid.

Example 3: Anionic synthesis of a polystyrene terminated by N-benzylidene tert-butylamine in a more concentrated solution than in Example 1



Drying of the vessel:

To a 300 ml four-necked flat-bottomed flask fitted with a mechanical stirrer, a reflux condenser and a thermometer are added distilled cyclohexane (100 ml) and styrene (1 g) under an argon atmosphere. The mixture is then heated to 60°C and 2 ml of sec-butyllithium (Aldrich; 1.3 M) are added. The polymerization medium becomes orange and, after 30 minutes, the polymerization medium is removed. Then, the reactor is filled with argon and washed with 50 ml of distilled cyclohexane.

Polymerization:

To the dried reactor are added 200 ml cyclohexane and 20 g of styrene (0.192 mol), and the temperature is increased to 40°C under an argon atmosphere. The polymerization of styrene is initiated by the addition of 15.4 ml of sec-butyllithium (Aldrich; 1.3 M; 0.02 mol). The polymerization medium becomes orange and the temperature increases to 64.4°C (in an exothermic reaction). After a reaction time of

1 h, the temperature is 41.1°C and 3.22 g of N-benzylidene tert-butylamine (0.02 mol) are added. The polymerization medium rapidly becomes colourless. After 30 minutes at 41.1°C, 3.1 ml of isopropanol (0.04 mol) are added. The organic solution is then washed once with 200 ml of water, twice with 200 ml of 1N HCl and once with 200 ml of water and it is then dried with Na₂SO₄, filtered and finally the solvent and residual monomer are removed in vacuo at 70°C. 22.72 g of **1'** are collected as a white solid.

The molecular characteristics of **1'** as measured by GPC are as follows:

Mn = 1054 g/mol

Mw = 1140 g/mol

Mw/Mn = 1.08

Example 4: Copolymerization of styrene and acrylonitrile in the presence of **1'** synthesized in Example 3 and peracetic acid, according to the present invention

To a 100 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel is added 0.096 g of peracetic acid (Aldrich, 35 wt.%; $4.418 \cdot 10^{-4}$ mol). Then a mixture of 0.5 g of **1'**, 14.67 g of styrene (0.141 mol) and 4.89 g of acrylonitrile (0.092 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at room temperature, the mixture is heated under reflux for 2 h. Samples are extracted from the reaction flask after 1 and 2 h and dried in vacuo at 50°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

Table 4 shows the results obtained by GPC.

Table 4: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
1	15.9	24420	34540	1.41
2	71.7	59780	86240	1.44

The increase in the molecular weight of the polymer with the monomer conversion and the narrow polydispersity are consistent with a controlled process.

Additionally, in contrast to the other NMP systems actually reported in the literature, the polymerization of SAN in the presence of **1'** and peracetic acid, in the absence of any additional initiator, takes place very quickly (and is almost complete after 2.5 h).

10

Example 5: Copolymerization of styrene and acrylonitrile in the presence of **1'** synthesized in Example 3 and peracetic acid: synthesis of controlled high molecular weight SAN

To a 250 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel is added 0.192 g peracetic acid (Aldrich, 35 wt.%; $8.83 \cdot 10^{-4}$ mol). Then, a mixture of 1 g of **1'**, 58.68 g styrene (0.563 mol) and 19.56 g acrylonitrile (0.369 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at room temperature, the mixture is heated under reflux for 5.2 h. Samples are extracted from the reaction flask after 1.5 h, 4 h, and 5.33 h and dried in vacuo at 50°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

The results obtained are summarized in Table 5.

25

Table 5: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
1.5	16.9	49930	77980	1.56
4	48.2	82280	129200	1.57
5.33	71.7	112600	181700	1.61

5 The increase in the molecular weight of the polymer with the monomer conversion and the narrow polydispersity are consistent with a controlled process. Controlled high molecular weight SAN can be synthesized in a short reaction time using **1'**.

Comparative example C: Copolymerization of styrene and acrylonitrile in the presence of TEMPO

10

To a 100 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel, a mixture of 0.0548 g of TEMPO ($3.5 \cdot 10^{-4}$ mol), 29.34 g styrene (0.563 mol) and 9.78 g acrylonitrile (0.369 mol) is added. The mixture is stirred and degassed by bubbling through argon for 10 minutes. Then,
15 the mixture is heated under reflux for 2.25 h. Samples are extracted from the reaction flask after 2 h, 12 h and 24 h and dried in vacuo at 50°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

20

The results obtained are summarized in Table 6.

Table 6: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
2	0,3	-	-	-
12	25.6	26120	36470	1.39
24	64.8	44440	73930	1.66

5 The polymerization is very slow (only traces of polymer are obtained after 2 h of polymerization) and an only 64.8 % monomer conversion is obtained after a reaction time of 24 h.

Example 6: Copolymerization of n-butylacrylate, styrene and acrylonitrile in the presence of **1'** synthesized in Example 3 and peracetic acid

10

To a 100 ml four-necked round bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel, 0.192 g of peracetic acid (Aldrich, 35 wt.%; $8.83 \cdot 10^{-4}$ mol) is added. Then a mixture of 1 g of **1'**, 19.56 g of n-butyl acrylate (0.152 mol), 14.67 g styrene (0.141 mol) and 4.89 g of acrylonitrile (0.092 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at room temperature, the mixture is heated at 110°C for 4 h. Samples are extracted from the reaction flask after 1 h, 2 h, and 4 h and dried in vacuo at 80°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

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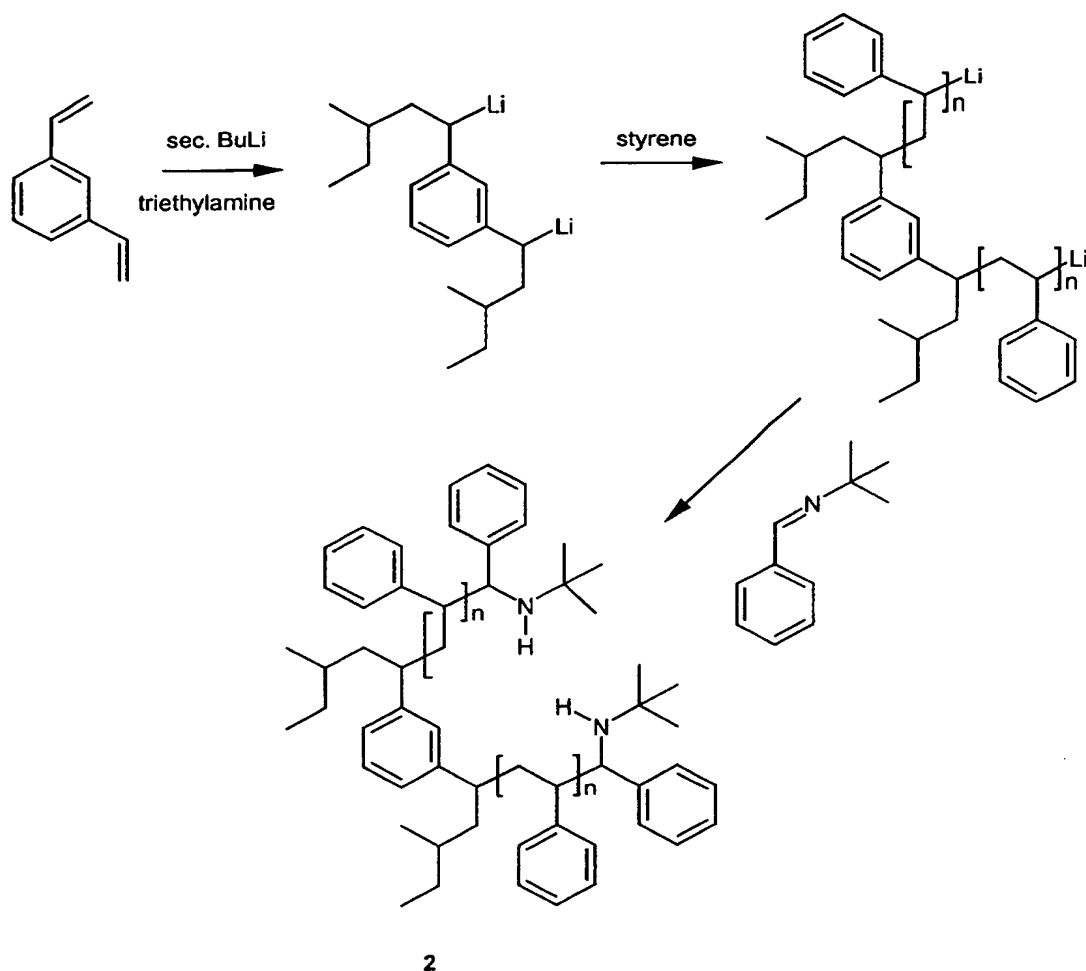
The results obtained are summarized in Table 7.

Table 7: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
1	21.1	32090	50200	1.56
2	50.0	54100	82470	1.52
4	76.5	73370	129000	1.75

5 The increase in the molecular weight of the polymer with the monomer conversion and the narrow polydispersity are consistent with a controlled process. Additionally, the copolymerization takes place rapidly without the addition of any activator: 76.5 % monomer conversion after 4 h at a low temperature (110°C).

10 **Example 7:** Anionic synthesis of a polystyrene terminated by N-benzylidene tert-butylamine at both chain ends



Drying of the vessel:

To a 300 ml four-necked flat-bottomed flask fitted with a mechanical stirrer, a reflux condenser and a thermometer are added distilled cyclohexane (100 ml) and styrene (1 g) under an argon atmosphere. The temperature is then heated at 60°C and 2 ml of *sec*-butyllithium (Aldrich; 1.4 M) are added. The polymerization medium becomes orange and after 30 minutes is removed. Then the reactor is filled with argon and washed with 50 ml of distilled cyclohexane.

Polymerization:

To the dried reactor, 200 ml of cyclohexane and 14.3 ml of sec-butyllithium (Aldrich; 1.4 M) are added. The solution is heated at 40°C and 2 ml of dried triethylamine (1 M in cyclohexane) are added. A solution of divinylbenzene in cyclohexane (1.3 g in 10 ml cyclohexane; 0.01 mol; 0.5 eq. based on sec-butyllithium) is then added slowly to the reaction flask over a period of 15 minutes. The reaction solution becomes deep red. After 30 min. at 40°C, 20 g of styrene (0.192 mol) are added and the reaction is stirred for 30 min. at 60°C. After this period of time, 3.23 g of N-benzylidenes tert-butylamine (0.02 mol) are added. The polymerization medium becomes rapidly colourless. After 30 minutes at 60°C, 2 ml of isopropanol (0.026 mol) are added. The organic solution is then washed twice with 200 ml of HCl 1N, once with 100 ml of water and twice with 200 ml of NaOH 1N and it is then dried with Na₂SO₄, filtered and finally, the solvent and residual monomer are removed in vacuo at 70°C. 24.33 g of **2** are collected as a white solid.

The molecular characteristics of **2** as measured by GPC are as follows:

M_n = 1946
M_w = 2348
M_w/M_n = 1.20

Example 8: Copolymerization of styrene and acrylonitrile in the presence of **2** synthesized in Example 7 and peracetic acid.

To a 100 ml four-necked round bottomed flask fitted with a mechanical stirrer, a reflux condenser, a thermometer and a funnel 0.222 g of peracetic acid (Aldrich, 35 wt.%; 1 10⁻³ mol) is added. Then, a mixture of 1 g of **2**, 29.34 g of styrene (0.281 mol) and 9.78 g of acrylonitrile (0.184 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at room temperature, the mixture is heated under reflux for 2 h. Samples

are extracted from the reaction flask after 1 h and 2 h and dried in vacuo at 50°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

5 The results obtained are summarized in Table 8.

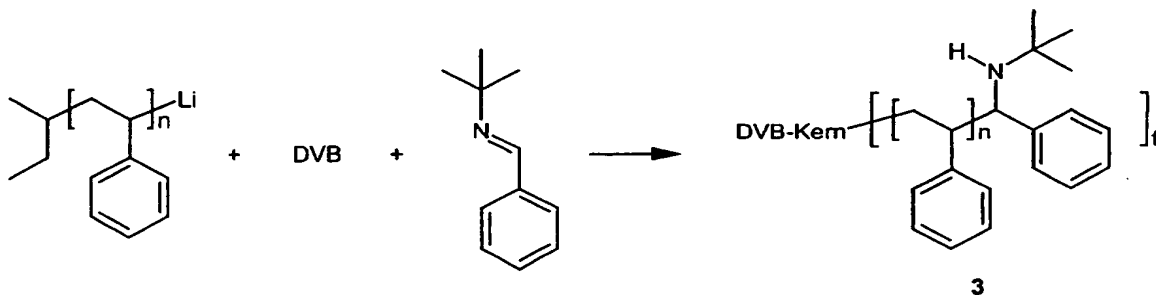
Table 8: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
1	20.3	43500	70000	1.61
2	73.2	80000	132400	1.65

10 Controlled polymerization is observed, as shown by the increase in the molecular weight with the monomer conversion and the narrow polydispersity.

Surprisingly, although high molecular weight SAN is formed, the polymerization takes place very rapidly compared to the conventional NMP process: after only 2
15 under reflux, a 72,3% monomer conversion is obtained.

Example 9: Anionic synthesis of a star-like polystyrene terminated by N-benzylidene tert-butylamine at each arm-ends



Drying of the vessel:

To a 300 ml four-necked flat-bottomed flask fitted with a mechanical stirrer, a reflux condenser and, a thermometer are added distilled cyclohexane (100 ml) and styrene (1 g) under an argon atmosphere. The mixture is then heated at 60°C and 2 ml of sec-butylolithium (Aldrich; 1.4 M) are added. The polymerization medium becomes orange and after 30 minutes, it is removed. Then the reactor is filled with argon and washed with 50 ml of distilled cyclohexane.

Polymerization:

To the dried reactor, 200 ml of cyclohexane and 14.3 ml of sec-butylolithium (Aldrich; 1.4 M) are added. The solution is heated at 40°C and 2 ml of dried triethylamine (1 M in cyclohexane) are added. A solution of divinylbenzene in cyclohexane (1.95 g divinylbenzene dissolved in 10 ml cyclohexane) is then added slowly for 15 minutes to the reaction flask. After 30 min. at 40°C, 20 g of styrene (0.192 mol) are added and the reaction is continued for 30 min. at 60°C. After this period of time, 3.23 g of N-benzylidene tert-butylamine (0.02 mol) are added. The polymerization medium rapidly becomes colourless. After 30 minutes at 60°C, 2 ml of isopropanol (0.026 mol) are added. The organic solution is then washed twice with 200 ml of HCl 1N, once with 100 ml of water and twice with 200 ml of NaOH 1N and it is then dried with Na₂SO₄, filtered and finally, the solvent and residual monomer are removed in vacuo at 70°C. 24.52 g of **3** are collected as a white solid.

The molecular characteristics of **3** as measured by GPC are as follows:

M_n = 2795
M_w = 3603
M_w/M_n = 1.28

Example 10: Copolymerization of styrene and acrylonitrile in the presence of **3** synthesized in Example 9 and peracetic acid.

To a 100 ml four-necked round-bottomed flask fitted with a mechanical stirrer, a
5 reflux condenser, a thermometer and a funnel 0.2336 g peracetic acid (Aldrich,
35 wt.%; $1 \cdot 10^{-3}$ mol) is added. Then, a mixture of 1 g of **3**, 14.67 g styrene (0.14 mol)
and 4.89 g acrylonitrile (0.092 mol) is rapidly added via the funnel. The mixture is
stirred and degassed by bubbling through argon for 10 minutes. After 30 minutes at
room temperature, the mixture is heated under reflux for 3 h. Samples are extracted
10 from the reaction flask after 2 h and 3 h and dried in vacuo at 50°C for 24 h. The
monomer conversion is determined by gravimetric analysis and the molecular weight
of the polymer is determined by GPC.

The results obtained are summarized in Table 9.

15

Table 9: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
2	60.4	64300	106900	1.66
3	79.5	76200	143700	1.88

The increase in the molecular weight with the monomer conversion and the narrow
polydispersity are indicative of a controlled process. Moreover and surprisingly,
20 polymerization takes place very rapidly (a monomer conversion of approx. 80% after
only 3 h under reflux).

Example 11: Copolymerization of styrene and acrylonitrile in the presence of 3 synthesized in Example 9 and peracetic acid.

To a 1 litre four-necked round-bottomed flask fitted with a mechanical stirrer, a
5 reflux condenser, a thermometer and a funnel, 3.58 g peracetic acid (Aldrich, 35 wt.%; $1.64 \cdot 10^{-2}$ mol) are added. Then a mixture of 15.337 g of 3, 450 g of styrene (4.32 mol) and 150 g of acrylonitrile (2.82 mol) is rapidly added via the funnel. The mixture is stirred and degassed by bubbling through argon for 10 minutes. After 30
10 minutes at room temperature, the mixture is heated under reflux for 8 h. Then, the reaction is stopped and the polymer is dried in vacuo at 60°C for 24 h. The monomer conversion is determined by gravimetric analysis and the molecular weight of the polymer is determined by GPC.

The results obtained are summarized in Table 10.

15

Table 10: Results of GPC

Time (h)	Conversion (%)	M_n	M_w	M_w/M_n
8	58.48	176000	298300	1.69

A high molecular weight SAN is synthesized with a narrow polydispersity.

20

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1. Process for the preparation of oligomers, cooligomers, polymers or block or random copolymers comprising

5

(I) mixing compounds consisting essentially of

- a) at least one monoethylenically unsaturated monomer of the general formula (M),

10



wherein

15

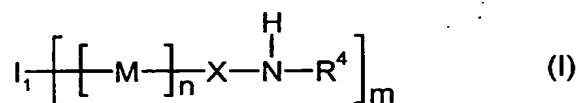
R^1 , R^2 , R^3 are independently selected from the group consisting of hydrogen, C_1 - C_{20} -alkyl, C_1 - C_{20} -cycloalkyl, C_6 - C_{24} -aryl, halogen, cyano, C_1 - C_{20} -alkylester, C_1 - C_{20} -cycloalkylester, C_1 - C_{20} -alkylamide, C_1 - C_{20} -cycloalkylamide, C_6 - C_{24} -arylester or C_6 - C_{24} -arylamide,

20

- b) at least one oxidizing agent (A) and

- c) at least one polymer or oligomer of the general formula (I),

25



wherein

R^1, R^2, R^3 have the aforesaid meaning,

m is an integer between 1 and 50,

5 n is an integer between 1 and 300 and

I_1 represents an initiator and

10 R^4 represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -alkyl, C_2 - C_{18} -alkenyl, C_2 - C_{18} -alkynyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl, C_6 - C_{24} -aryl, which may be unsubstituted or substituted by NO_2 , halogen, amino, hydroxy, cyano, carboxy, ketone,
15 C_1 - C_4 -alkoxy, C_1 - C_4 -alkylthio or C_1 - C_4 -alkylamino,

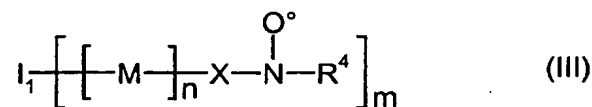
X represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -alkyl, C_2 - C_{18} -alkenyl, C_2 - C_{18} -alkynyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl, C_6 - C_{24} -aryl, which may be unsubstituted or substituted by NO_2 , halogen, amino, hydroxy, cyano, carboxy, ketone,
20 C_1 - C_4 -alkoxy, C_1 - C_4 -alkylthio or C_1 - C_4 -alkylamino,

25 d) optionally in the presence of a free radical initiator (B) and

(II) then heating the mixture at a temperature in the range from about $0^\circ C$ to about $220^\circ C$.

30

2. Process according to Claim 1, wherein a solvent selected from the group consisting of water, alcohols, esters, ethers, ketones, amides, sulfoxides, hydrocarbons and halogenated hydrocarbons is used.
- 5 3. Process according to Claim 1, wherein the monomers (M) are selected from the group consisting of styrene, substituted styrene, conjugated dienes, acrolein, vinyl acetate, acrylonitrile, methyl acrylate, methyl methacrylate, butyl acrylate, butyl methacrylate, 2-ethylhexyl acrylate, cyclohexyl methacrylate, isobornyl methacrylate and maleic anhydride.
- 10 4. Process according to Claim 1, wherein the oxidizing agent (A) is selected from the group consisting of peracetic acid, perpropionic acid, hydrogen peroxide, hydrogen peroxide/titanium containing catalysts, potassium peroxy-monosulfate ($2 \text{ KHSO}_5 \cdot \text{KHSO}_4 \cdot \text{K}_2\text{SO}_4$), silver oxide and lead (IV) oxide.
- 15 5. Process according to Claim 1, wherein the polymerization temperature in step (II) is between 50 and 180°C.
- 20 6. Process according to Claim 1, wherein the polymerization temperature in step (II) is between 70 and 150°C.
7. Process according to Claim 1, wherein the reaction temperature in step (I) is between 0 and 100°C.
- 25 8. Process according to Claim 1, wherein the reaction temperature in step (I) is between 0 and 50°C.
9. Process for the preparation of nitroxyl radicals of the general formula (III),



wherein

- 5 R^1, R^2, R^3 are independently selected from the group consisting of: hydrogen, C_1 - C_{20} -alkyl, C_1 - C_{20} -cycloalkyl, C_6 - C_{24} -aryl, halogen, cyano, C_1 - C_{20} -alkyl ester, C_1 - C_{20} -cycloalkyl ester, C_1 - C_{20} -alkylamide, C_1 - C_{20} -cycloalkylamide, C_6 - C_{24} -aryl ester or C_6 - C_{24} -arylamide,
- 10 m is an integer between 1 and 50, preferably between 1 and 20, and more preferably between 1 and 10,
- n is an integer between 1 and 300, preferably between 1 and 50, and more preferably between 1 and 20 and
- 15 I_1 represents an initiator and
- 20 R^4 represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -alkyl, C_2 - C_{18} -alkenyl, C_2 - C_{18} -alkynyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl, C_6 - C_{24} -aryl, which may be unsubstituted or substituted by NO_2 , halogen, amino, hydroxy, cyano, carboxy, ketone, C_1 - C_4 -alkoxy, C_1 - C_4 -alkylthio or C_1 - C_4 -alkylamino,
- 25 X represents a secondary or tertiary carbon atom and is independently selected from the group consisting of C_1 - C_{18} -alkyl, C_2 - C_{18} -alkenyl, C_2 - C_{18} -alkynyl, C_3 - C_{12} -cycloalkyl or C_3 - C_{12} -heterocycloalkyl, C_6 - C_{24} -aryl, which may be unsubstituted or substituted by NO_2 , halogen, amino, hydroxy, cyano, carboxy, ketone, C_1 - C_4 -alkoxy, C_1 - C_4 -alkylthio or C_1 - C_4 -alkylamino,

by mixing the polymer or oligomer of the general formula (I) with an oxidizing agent (A), followed by isolation of the compound of the general formula (III).

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10. A polymerizable composition containing

- d) at least one vinyl monomer or ethylenically unsaturated oligomer,
- e) at least one polymer or oligomer of the general formula (III) and
- 10 f) optionally a free radical initiator (B).

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The in situ polymerization of monoethylenically unsaturated monomers with oligomeric or polymeric secondary amines

A b s t r a c t

The present invention relates to a new process for the preparation of well-defined random and block polymers or copolymers using hindered secondary amine-oligomers or polymers.

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